

# **On the accurate determination of laminar burning velocity from constant-volume propagating spherical flames**

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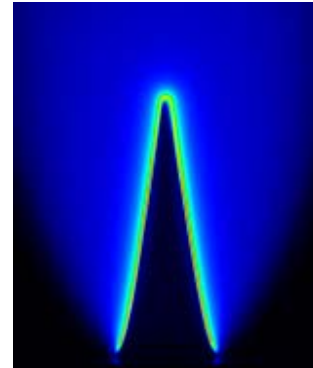


**3<sup>rd</sup> International Workshop on Laminar Burning Velocity, Lisbon, April 14, 2019**

# Laminar flame speed measurements

## Stationary flame method:

- Bunsen flame
- flat flame (heat flux method)
- counterflow or stagnation flame

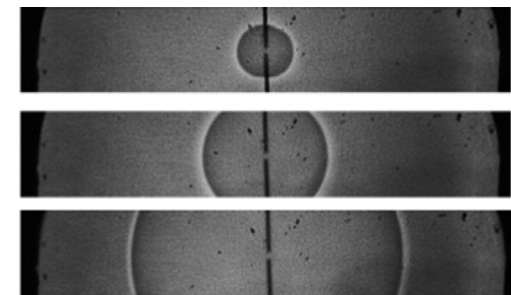


## Propagating flame method:

- cylindrical tube method
- soap bubble method
- propagating spherical flame method

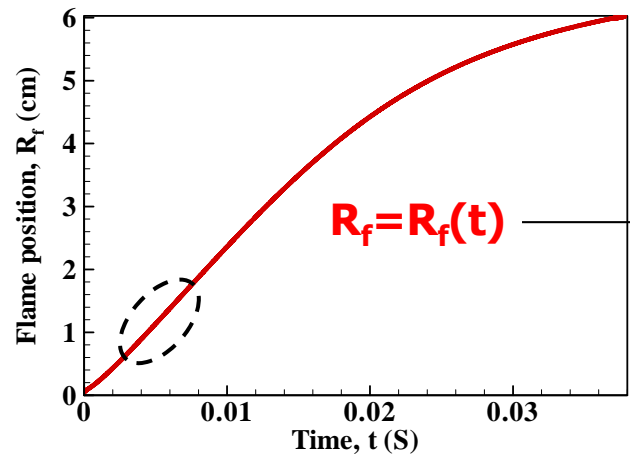
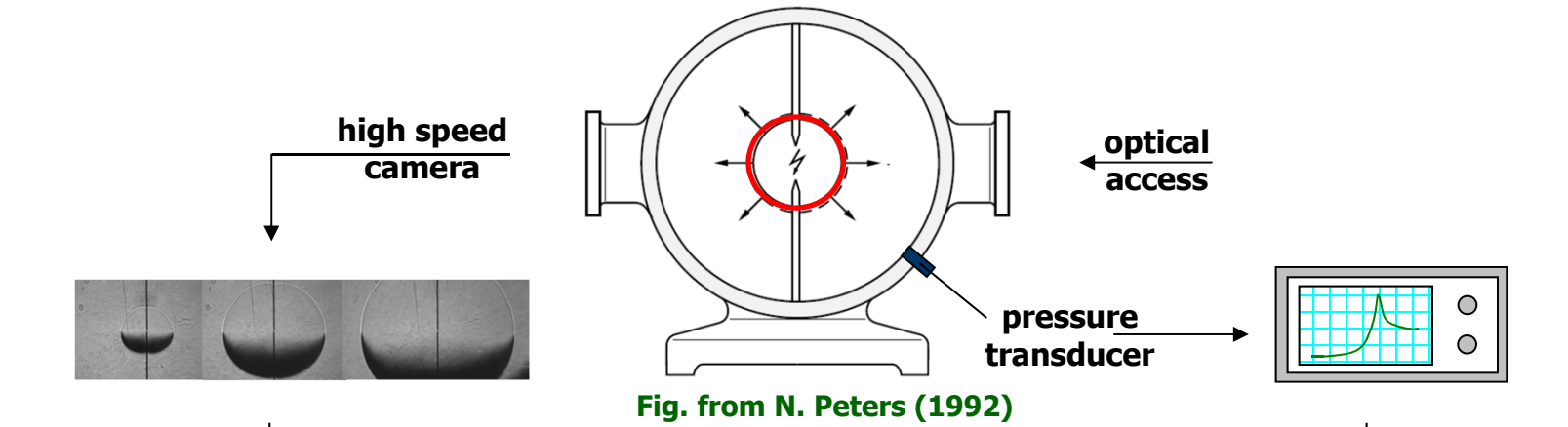


**High pressure & temperature !**



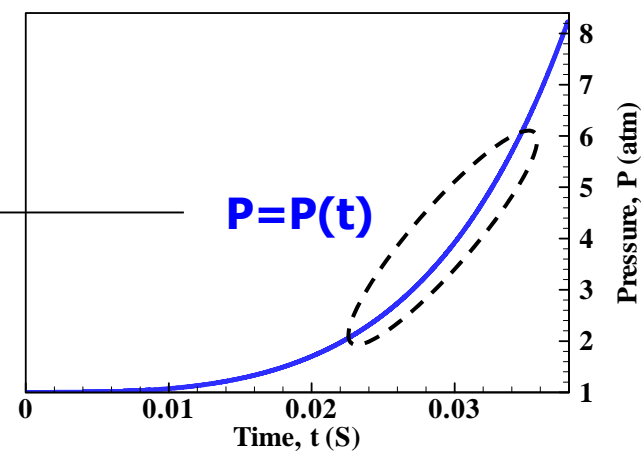
Figures from Egolfopoulos et al.,  
Prog. Energy Comb. Sci. 43 (2014).

# Propagating spherical flame method



**Constant-Pressure Method**  
 small flame, negligible P rise  
 Both  $S_u^0$  and Markstein length

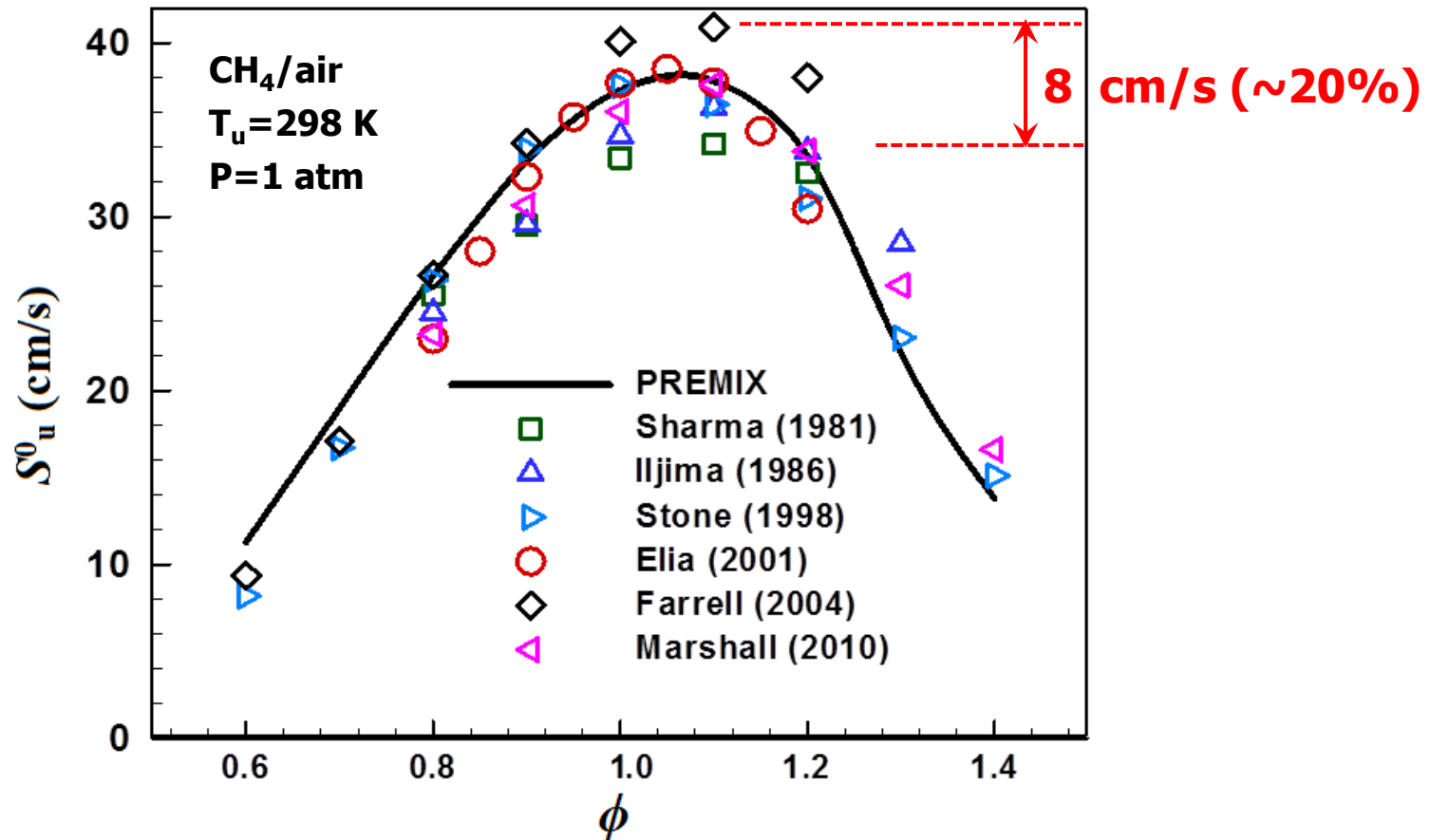
$S_u^0$



**Constant-Volume Method**  
 large flame with P rise  
 Engine-relevant  $T_u$  and P



# Data from the constant-volume method

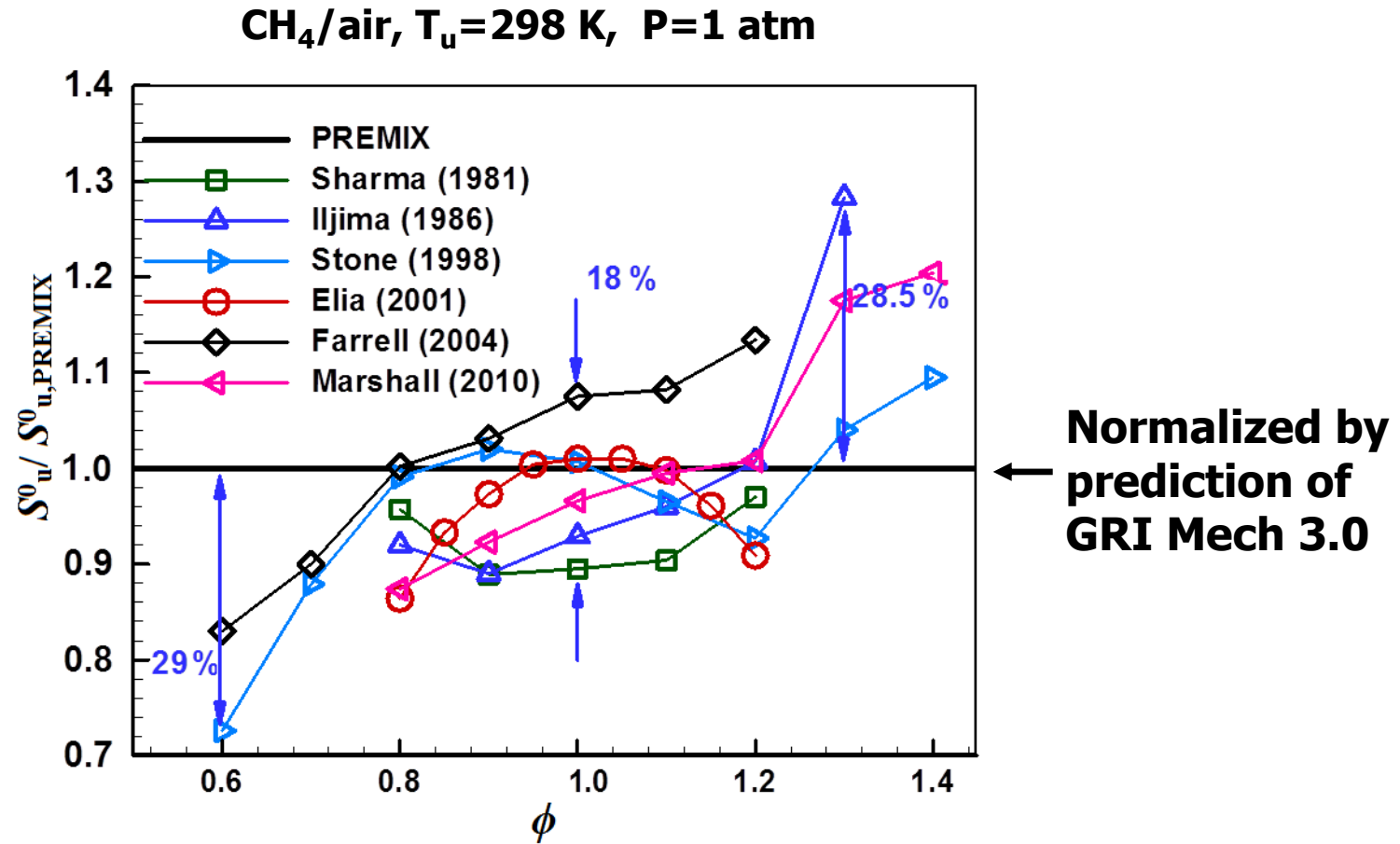


- **Same** constant-volume method for the **same** fuel CH<sub>4</sub>
- **Large discrepancy !**

M. Faghih, Z. Chen, The constant-volume propagating spherical flame method for laminar flame speed measurement, Science Bulletin, 61 (2016) 1296-1310.



# Discrepancy among $S_u^0$ measured by OPF

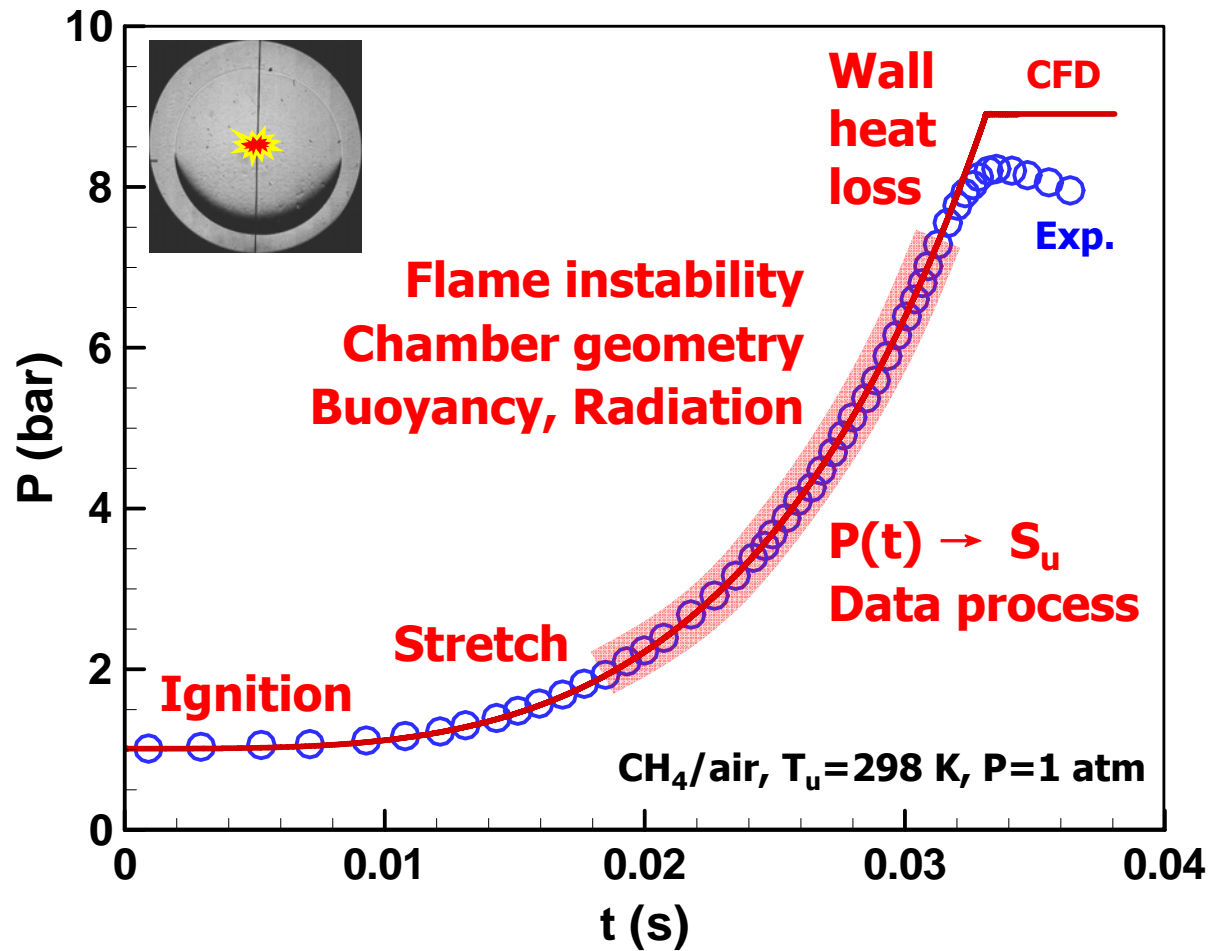


- Large discrepancy, **18%**, at  $\phi=1$
- Large discrepancy at **very lean or rich** conditions

M. Faghih, Z. Chen, The constant-volume propagating spherical flame method for laminar flame speed measurement, Science Bulletin, 61 (2016) 1296-1310.

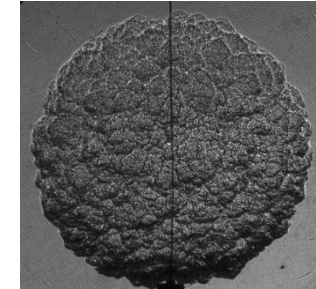
# Possible causes for uncertainty

Small radius  $\longrightarrow$  large radius



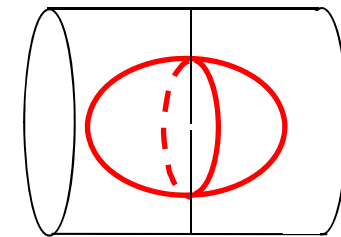
Symbols: Exp. (Movileanu et al. 2009); Line: CFD

## Flame instability

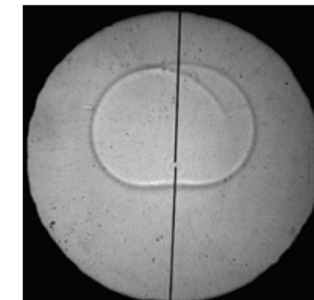


(Jomaas et al. 2013)

## Cylindrical chamber



## Buoyancy

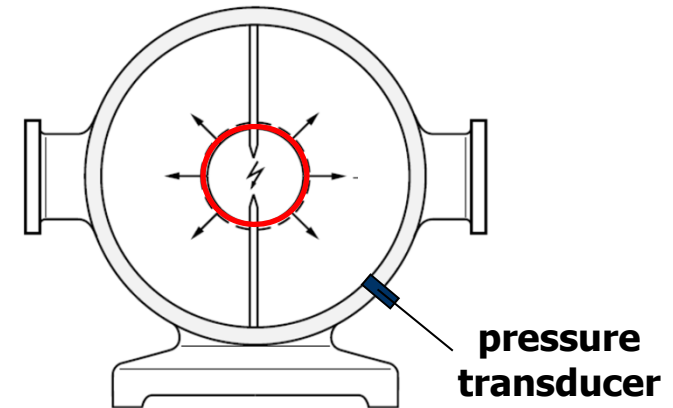


(Qiao et al. 2007)

# Data process

## Assumptions

- ❑ 1D spherical flame, no instability
- ❑ ideal gas, uniform pressure distribution
- ❑ isentropic compressed of unburned gas
- ❑ negligible radiation and buoyancy ...



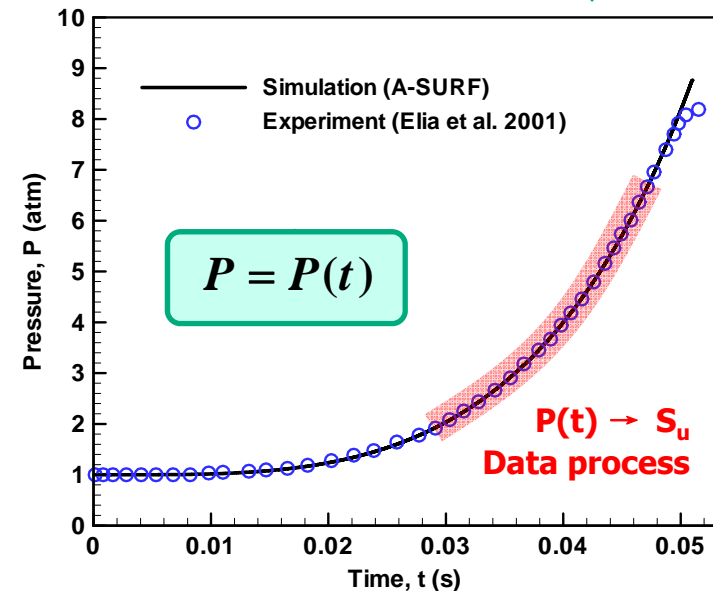
(N. Peters 1992)

$$S_u = \frac{dR_f}{dt} - \frac{R_W^3 - R_f^3}{3P\gamma_u R_f^2} \frac{dP}{dt}$$

$$\frac{R_f}{R_W} = \left[ 1 - (1-x) \left( \frac{P_0}{P} \right)^{1/\gamma_u} \right]^{1/3}$$

$$S_u = \frac{R_W}{3} \left[ 1 - (1-x) \left( \frac{P_0}{P} \right)^{1/\gamma_u} \right]^{-2/3} \left( \frac{P_0}{P} \right)^{1/\gamma_u} \frac{dx}{dt}$$

$$S_u = S_u(P) \quad T_u / T_{u,0} = (P / P_0)^{(1-1/\gamma_u)}$$



$x$ : burned mass fraction,  $x = m_b / m_0$ ,  $x = x(P)$



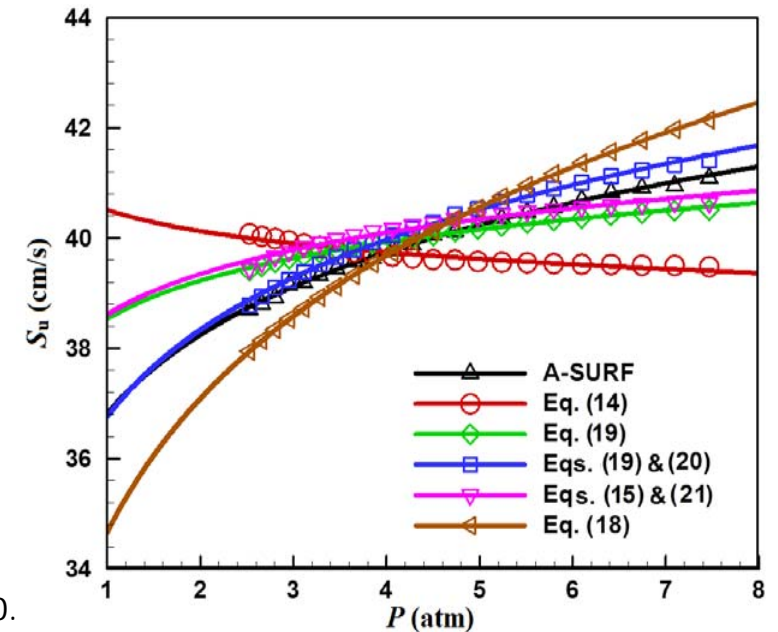
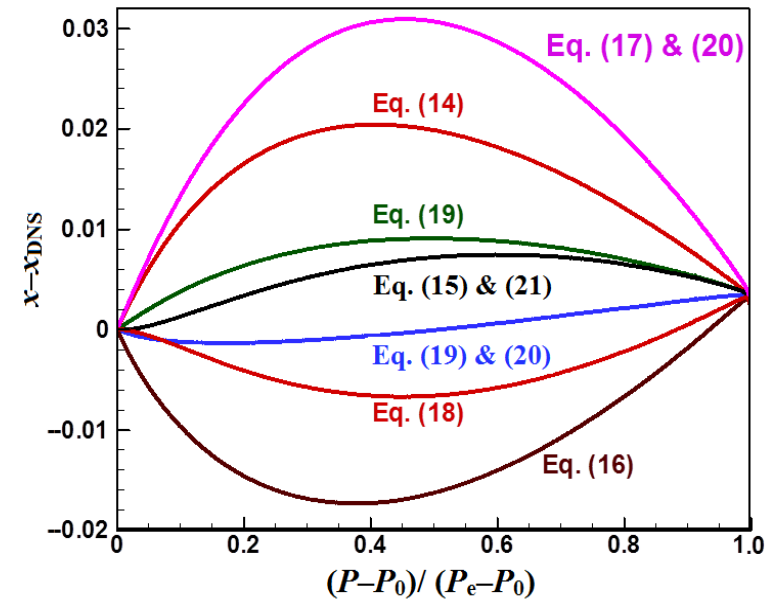
# Data process

CH<sub>4</sub>/air,  $\phi=1$ ,  $T_{u0}=300$  K,  $P_0=1$  atm

$$S_u = \frac{R_W}{3} \left[ 1 - (1-x) \left( \frac{P_0}{P} \right)^{1/\gamma_u} \right]^{-2/3} \left( \frac{P_0}{P} \right)^{1/\gamma_u} \frac{dx}{dt}$$

**x: burned mass fraction,  $x=m_b/m_0$ ,  $x=x(P)$**

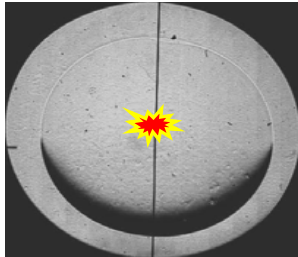
Correlation	Year	Eq. nos.
$x = \frac{(P-P_0)}{(P_c-P_0)}$	<b>Lewis &amp; von Elbe</b> 1951	(14)
$x(P) = \frac{(\bar{T}_c/\bar{T}_b)(P/P_0 - (P/P_0)^{(\gamma_u-1)/\gamma_u})}{P_c/P_0 - (\bar{T}_c/\bar{T}_b)(P/P_0)^{(\gamma_u-1)/\gamma_u}}$	1959	(15)
$x(P) = \frac{P-P_0(P/P_0)^{(\gamma_u-1)/\gamma_u}}{P_c-P_0(P/P_0)^{(\gamma_u-1)/\gamma_u}}$	1963	(16)
$x(P) = \frac{P^{1/\gamma_u} - P_0^{1/\gamma_u}}{P_c^{1/\gamma_u} - P_0^{1/\gamma_u}}$	1969	(17)
$x(P) = \frac{\alpha[(P/P_0)^{1/\gamma_u} - 1]}{(P/P_0)^{1/\gamma_u} - \alpha}$ , $\alpha = \frac{\rho_b^0}{\rho_0} + \frac{(1-\rho_b^0/\rho_0)(P/P_0-1)}{(P_c/P_0-1)}$	1980	(18)
$x = \frac{P-P_0f(P)}{P_c-P_0f(P)}$ , $f(P) = \frac{\gamma_b-1}{\gamma_u-1} + \frac{\gamma_u-\gamma_b}{\gamma_u-1} \left( \frac{P}{P_0} \right)^{(\gamma_u-1)/\gamma_u}$	<b>Luijten et al.</b> 2009	(19)
$x(P) = \frac{(\bar{T}_c/\bar{T}_b)(P/P_0 - (P/P_0)^{(\gamma_u-1)/\gamma_u})}{P_c/P_0 - (\bar{T}_c/\bar{T}_b)(P/P_0)^{(\gamma_u-1)/\gamma_u}}$ , $\bar{T}_c = \left( \frac{P_c}{P} \right)^{(\gamma^*-1)/\gamma^*}$ , $\gamma^* = \ln \left( \frac{P_c}{P_0} \left( 1 - \frac{T_{f,p}}{T_{f,v}} \right) \right)$	1994	(15), (21)
$x = \frac{P-P_0f(P)}{P_c-P_0f(P)}$ , $f(P) = \frac{\gamma_b-1}{\gamma_u-1} + \frac{\gamma_u-\gamma_b}{\gamma_u-1} \left( \frac{P}{P_0} \right)^{(\gamma_u-1)/\gamma_u}$ , $\gamma_{b,shift} = \frac{\gamma_b+8}{8}$	2016	(19), (20)



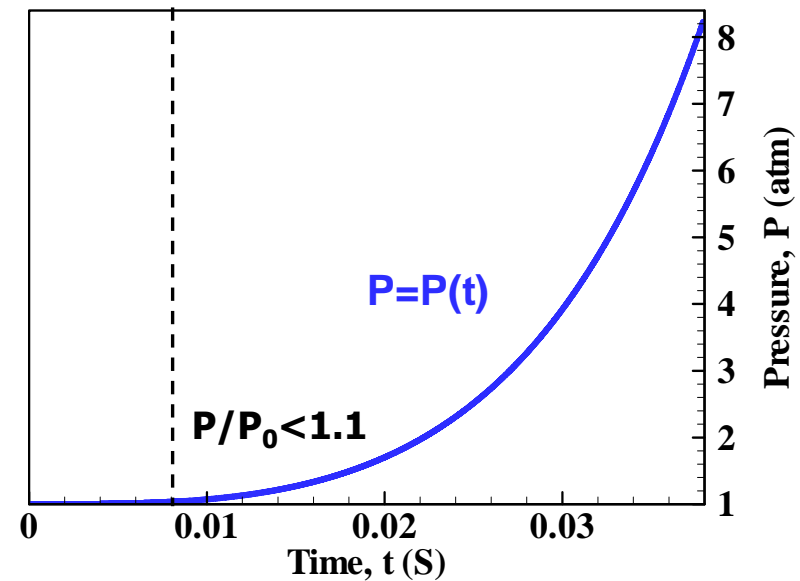
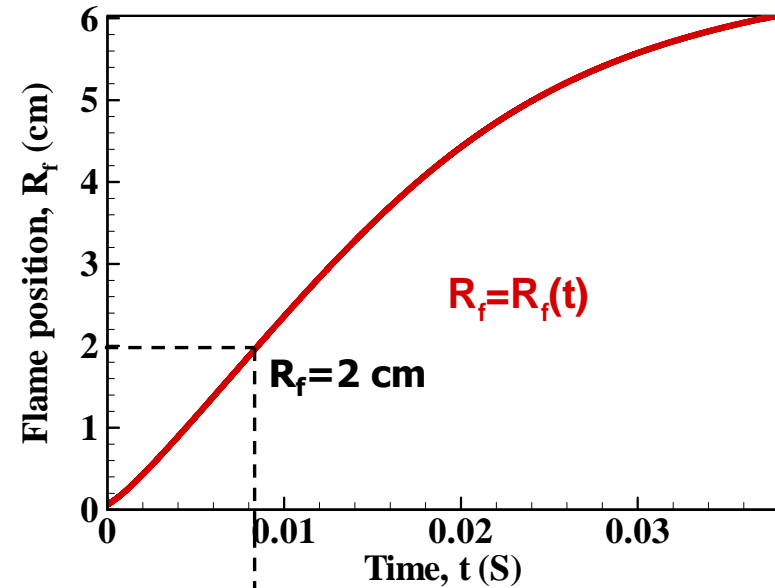
M. Faghih, Z. Chen, The constant-volume propagating spherical flame method for laminar flame speed measurement, Science Bulletin, 61 (2016) 1296-1310.



# Ignition



- Important for the constant-pressure method
- Negligible for the constant-volume method





# Stretch

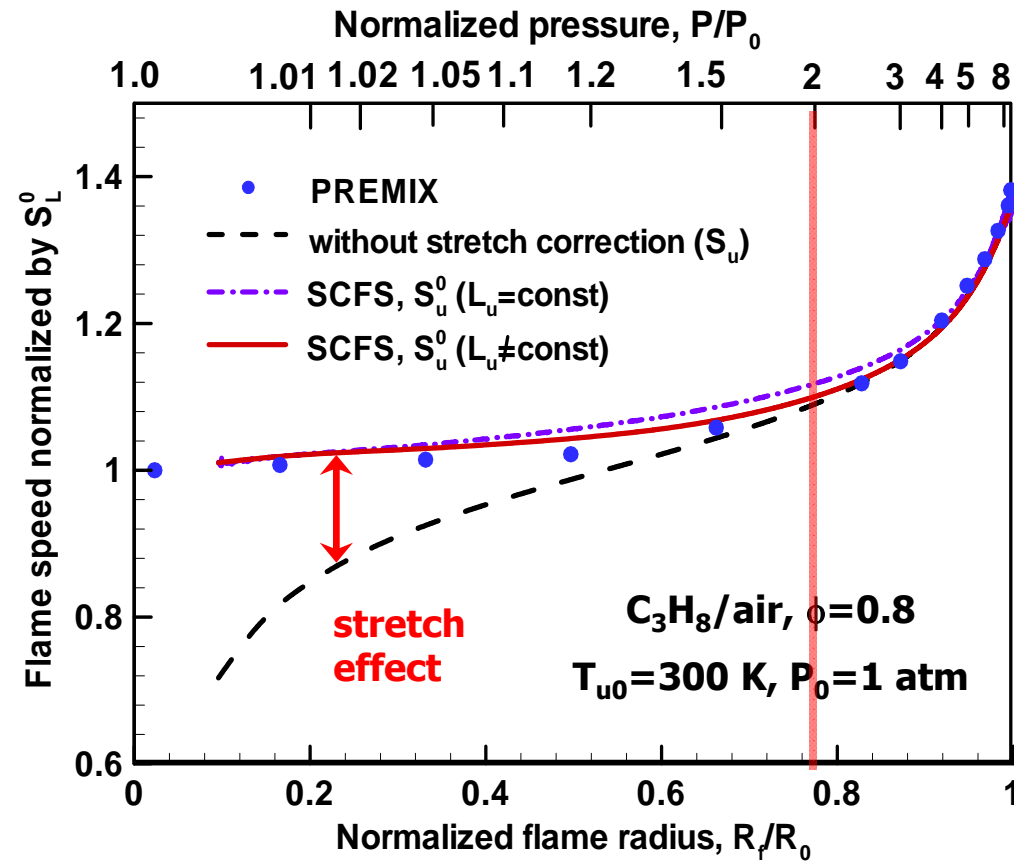
Chen et al. (2009CTM)

$$K = \frac{2}{R_f} \frac{dR_f}{dt}$$

$$S_u = S_u^0 - L_u K$$

$$\frac{S_u^0 - S_u}{S_u^0} \approx \frac{2L_u}{R_f} \left( \frac{\gamma_u - 1}{\gamma_u} + \frac{P_e}{\gamma_u P} \right)$$

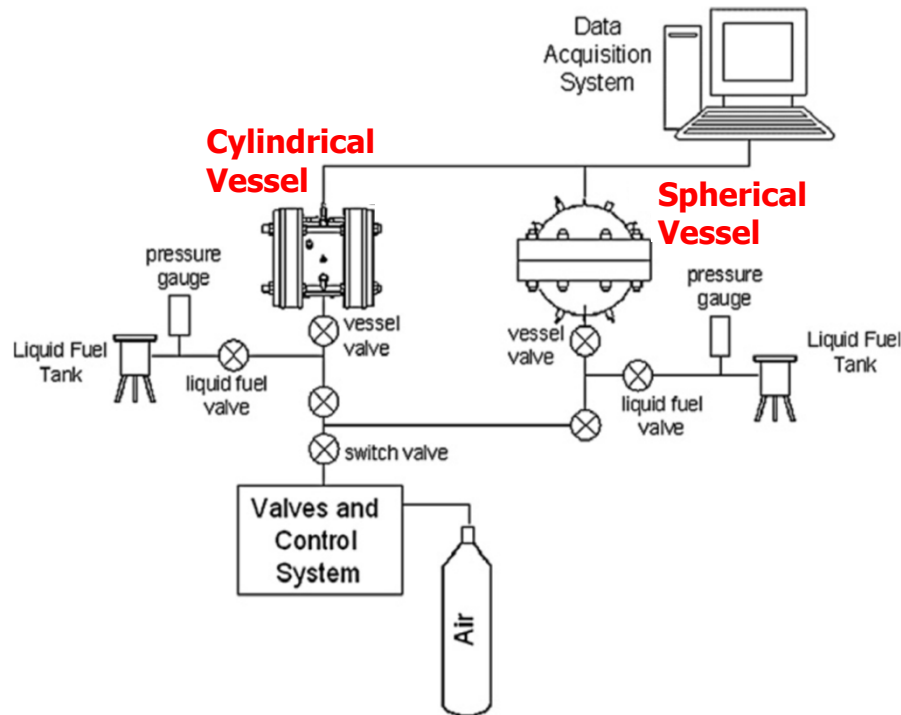
**Stretch effect**



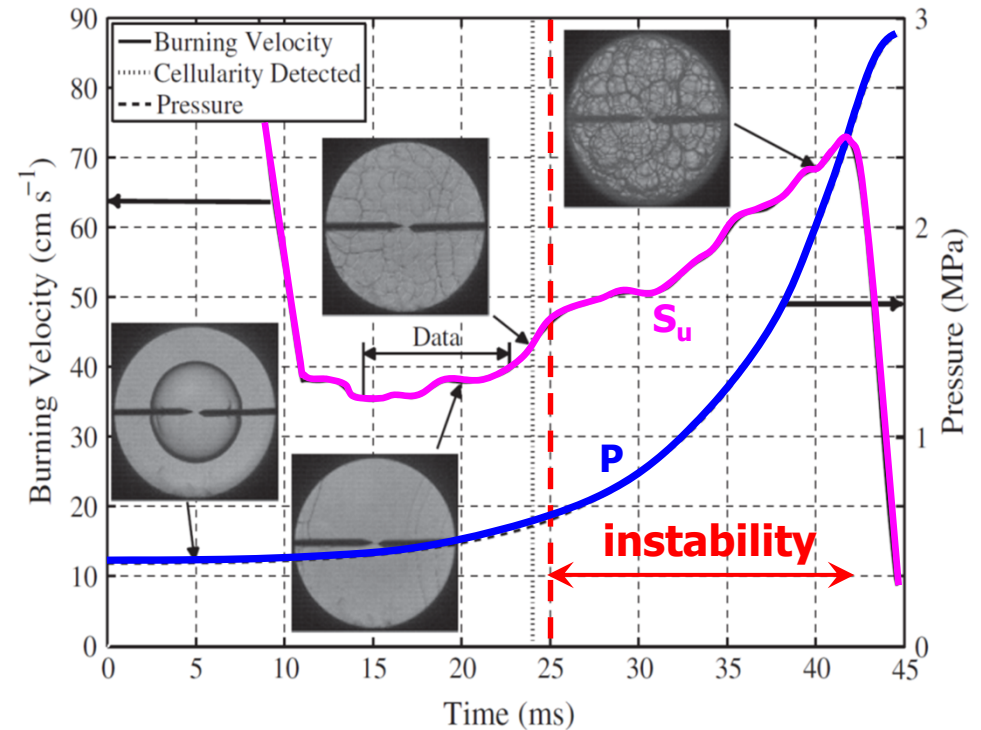
- Important only at the beginning; negligible for  $P/P_0 > 2$
- Negligible for high pressures

# Flame instability

18:17



Moghaddas et al. (2012CNF)



Marshall et al. (2011CNF)

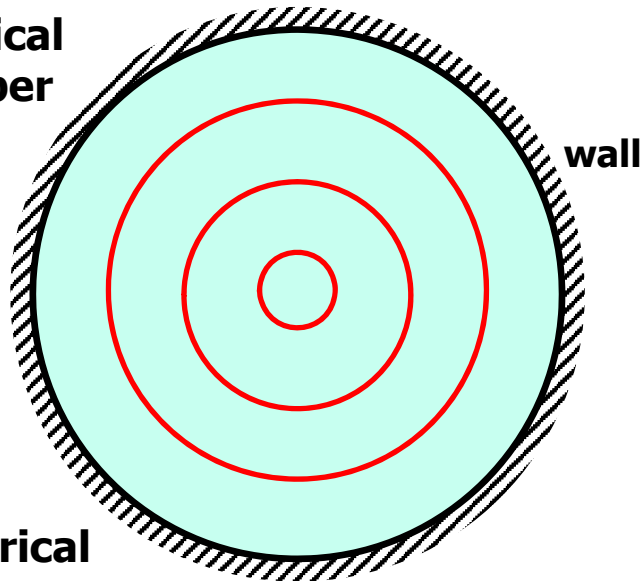
## ■ Two facilities:

- Cylindrical chamber, for full optical access and instability
- Spherical chamber, to preserve sphericity and record P

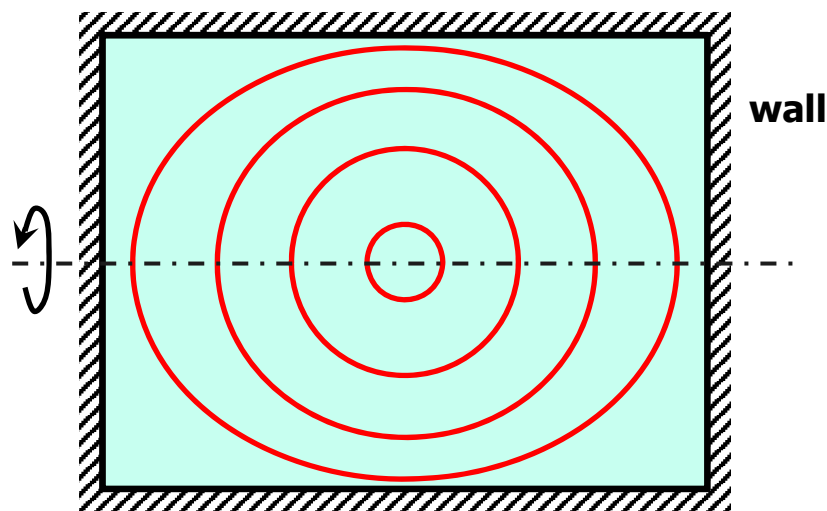
## ■ Single facility: spherical chamber + optical access (Fabien Halter)

# Chamber geometry

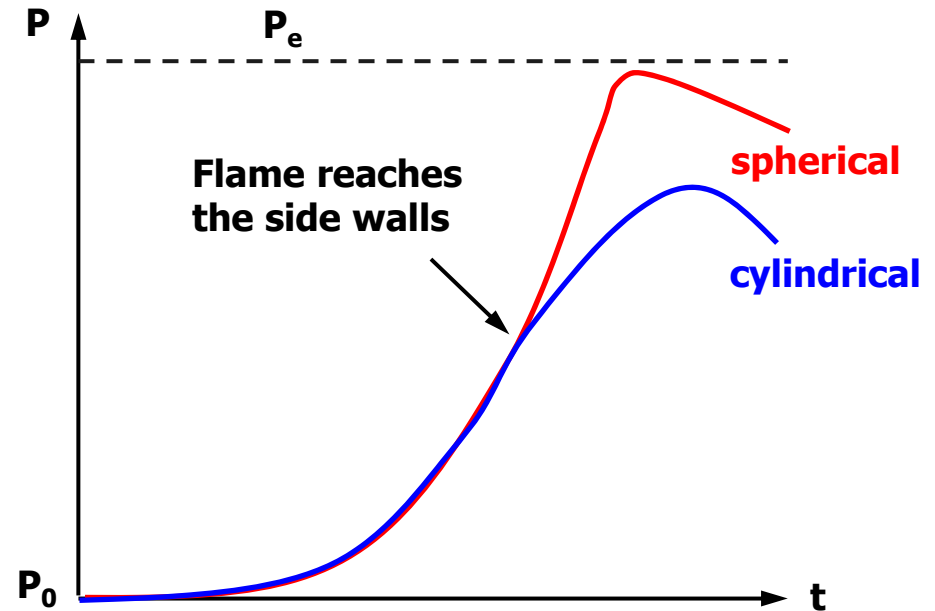
Spherical chamber



Cylindrical chamber



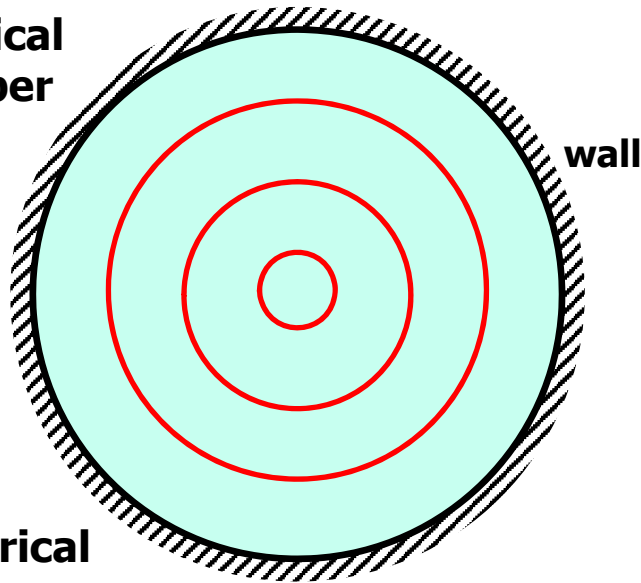
Burke et al. (2010CNF)



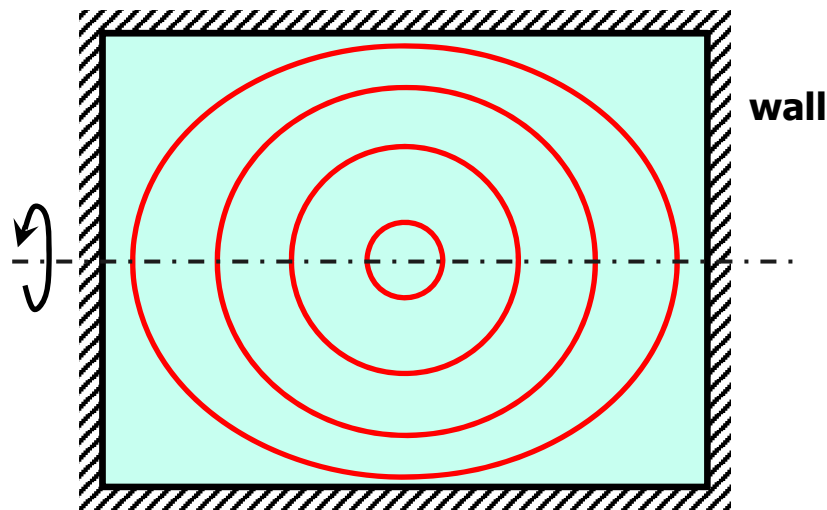
- For the cylindrical chamber, much lower  $P_{max}$  than  $P_e$
- Very close pressure history before flame reaches wall

# Chamber geometry

Spherical chamber

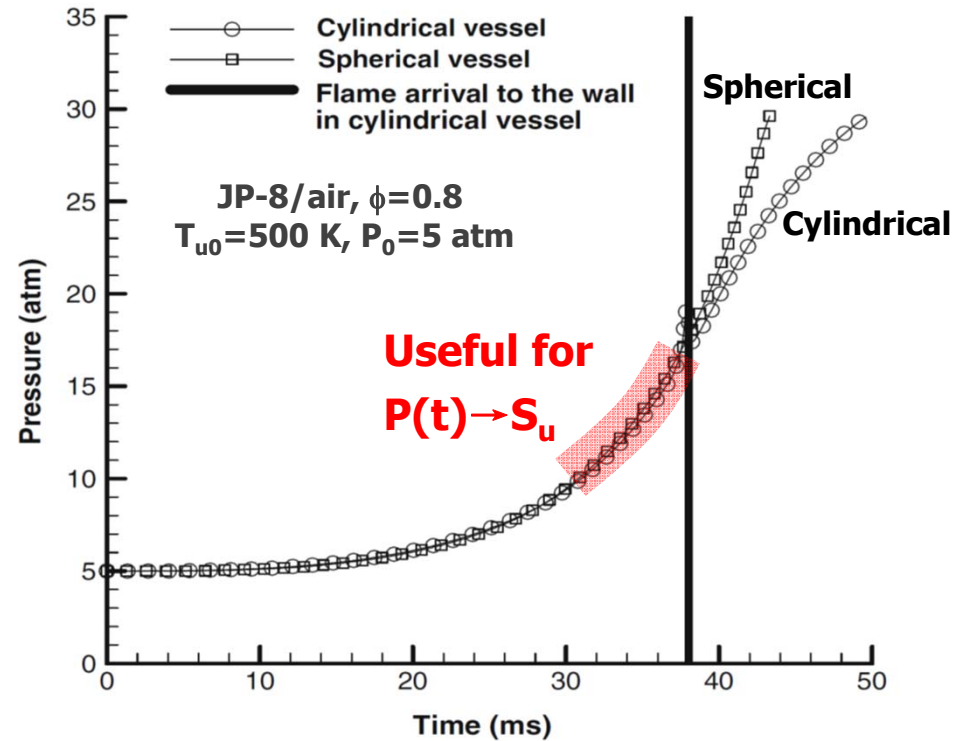


Cylindrical chamber



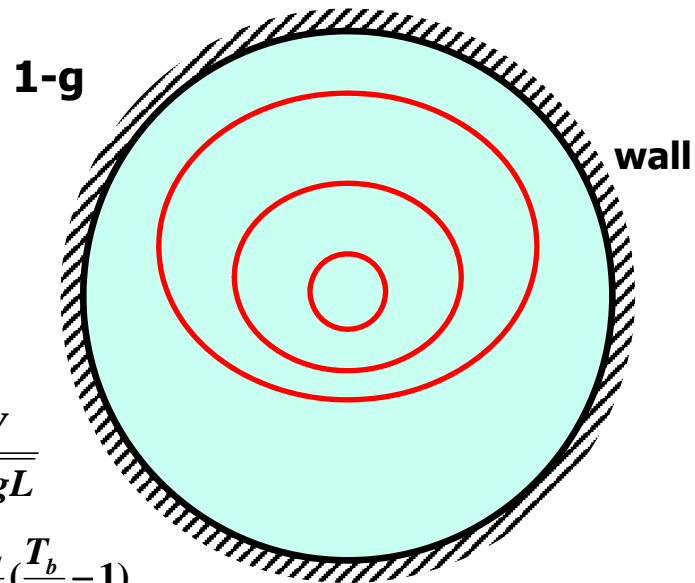
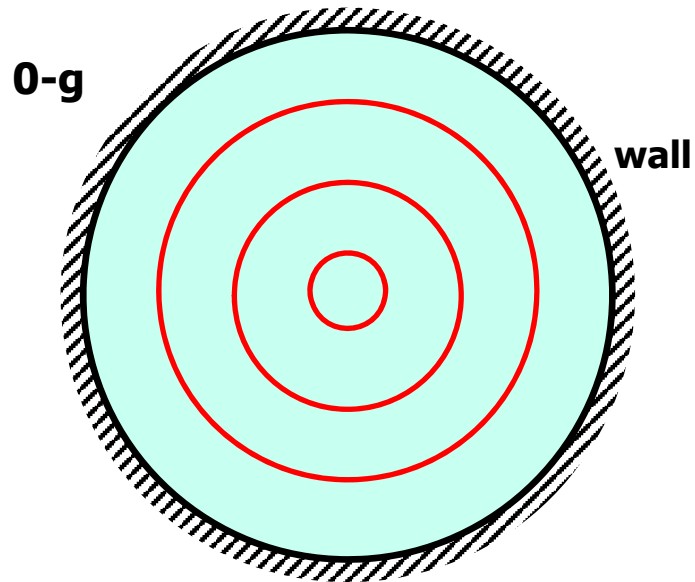
Burke et al. (2010CNF)

Exp. by Far et al. (2010Fuel)



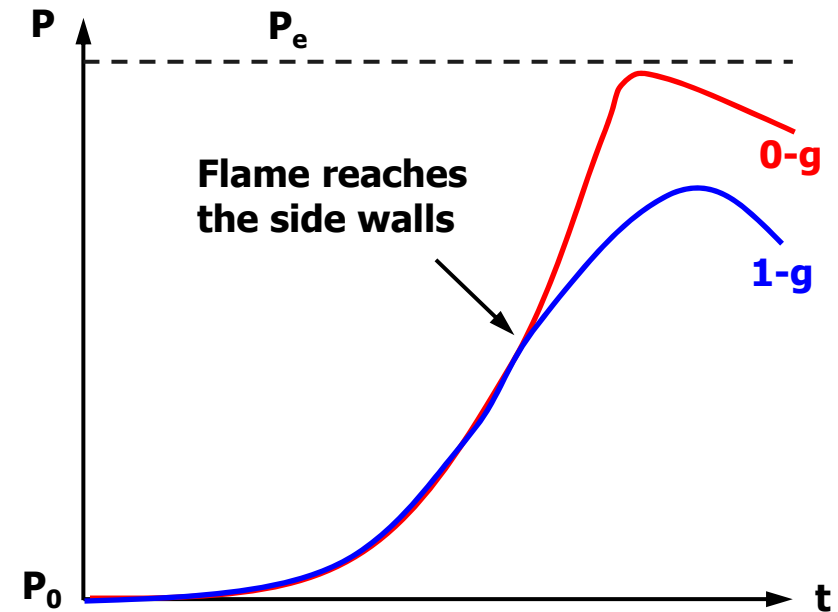
- For the cylindrical chamber, much lower  $P_{\max}$  than  $P_e$
- Very close pressure history before flame reaches wall

# Buoyancy



$$Fr = \frac{V}{\sqrt{gL}}$$

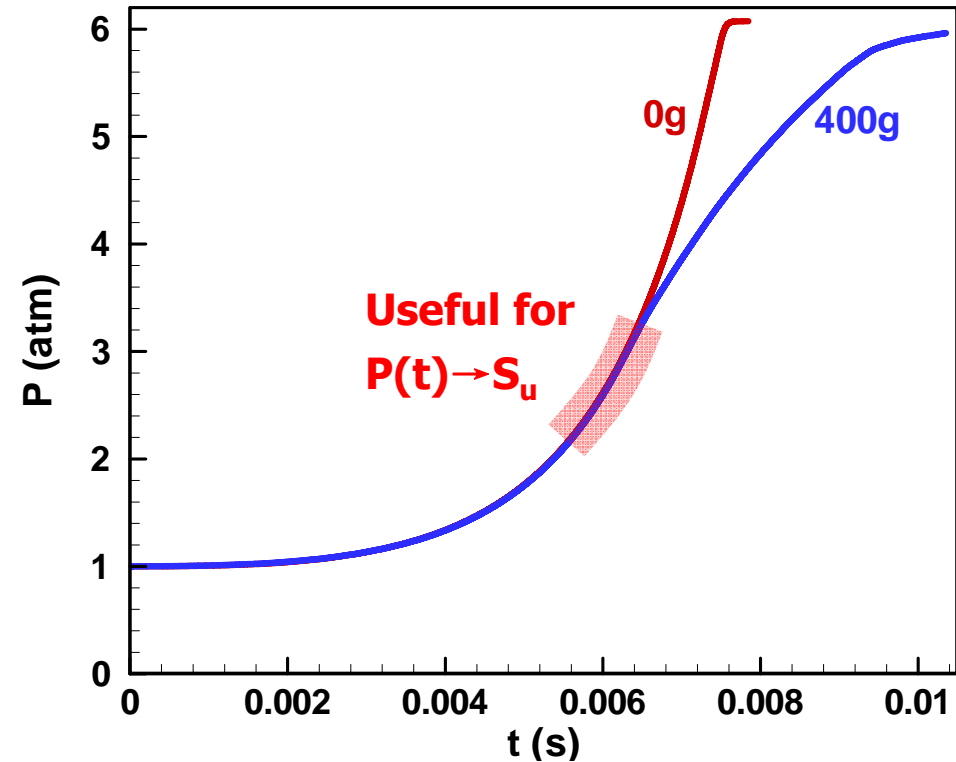
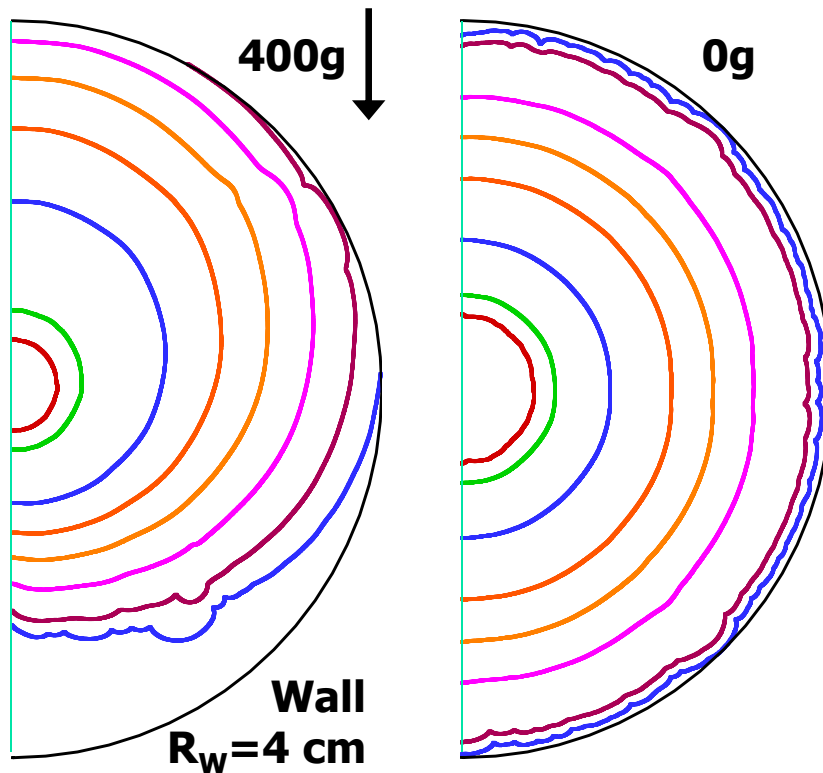
$$Ri = \frac{gL}{V^2} \left( \frac{T_b}{T_u} - 1 \right)$$



- Identical at 1-g and  $\mu$ -g for  $S_u^0 > 15$  cm/s (Ronney 1985)
- Similar pressure history before flame reaches wall
- Non-spherical ?

# Buoyancy

18:17

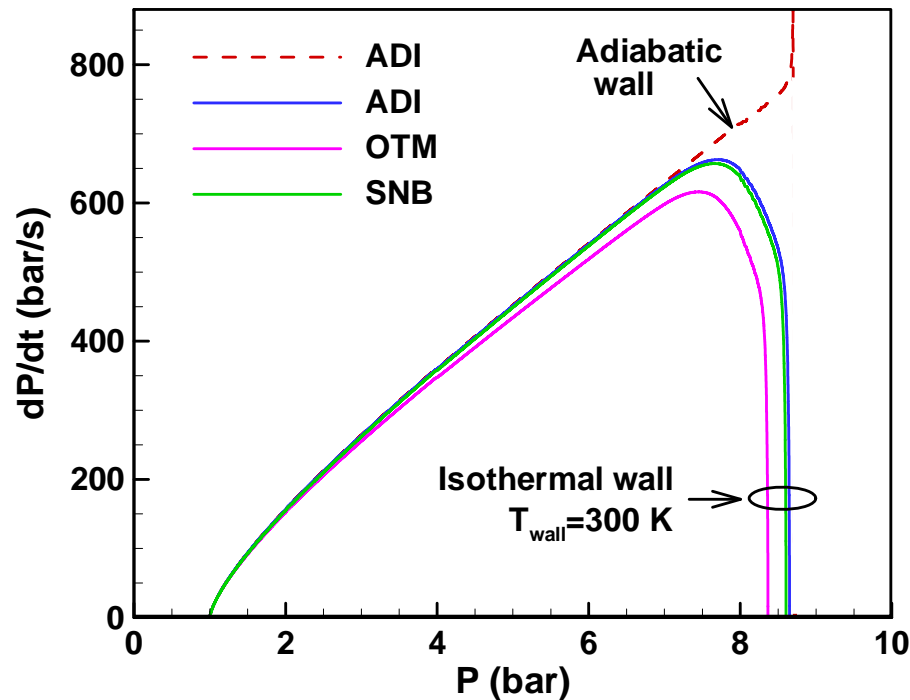


- 2D simulation by Fluent,  $H_2:O_2:N_2=6:1:4.96$ ,  $T_0=300$  K,  $P_0=1$ atm
- $S_u=170$  cm/s @ 400g is **equivalent** to  $S_u=8.5$  cm/s @ 1g

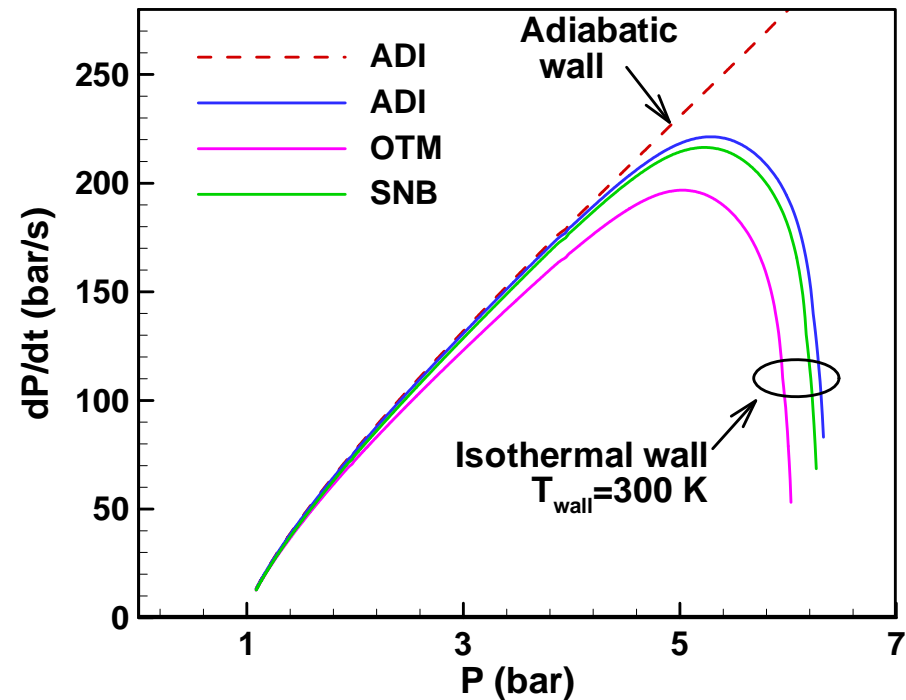
$$Ri = \frac{gL}{V^2} \left( \frac{T_b}{T_u} - 1 \right)$$

# Radiation

CH<sub>4</sub>/air,  $\phi=1.0$ ,  $T_{u0}=300$  K,  $P_0=1$  bar



CH<sub>4</sub>/air,  $\phi=0.6$ ,  $T_{u0}=300$  K,  $P_0=1$  bar



- Negligible even for weak mixture: within 2%
- Radiation absorption reduces the difference
- Slow burning fuels, e.g.: refrigerants ?



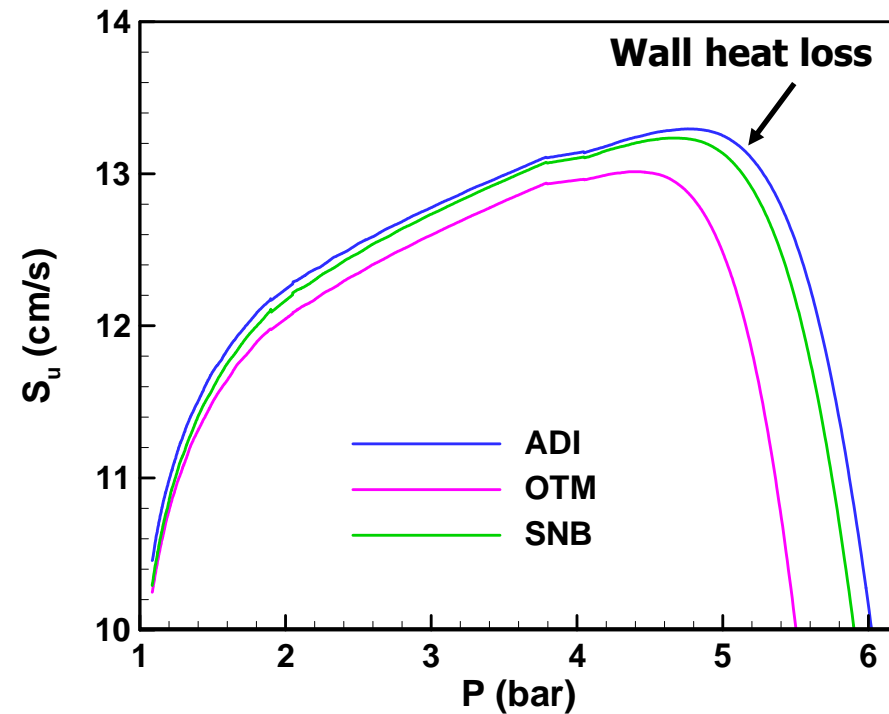
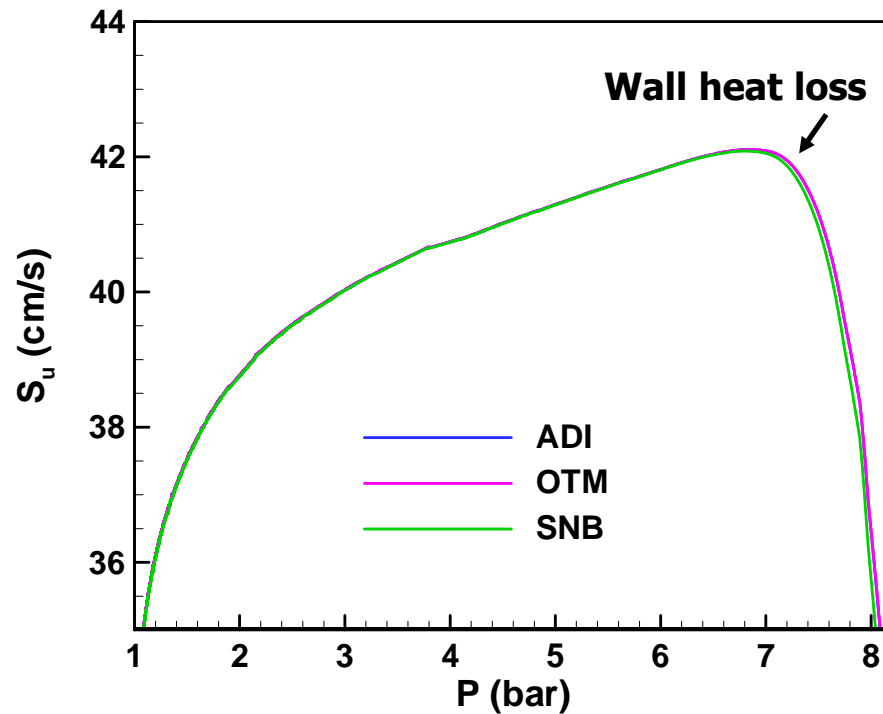
# Radiation

$$S_u = \frac{R_w}{3} \left[ 1 - (1-x) \left( \frac{P_0}{P} \right)^{1/\gamma_u} \right]^{-2/3} \left( \frac{P_0}{P} \right)^{1/\gamma_u} \frac{dx}{dt}$$



CH<sub>4</sub>/air,  $\phi=1.0$ , T<sub>u0</sub>=300 K, P<sub>0</sub>=1 bar

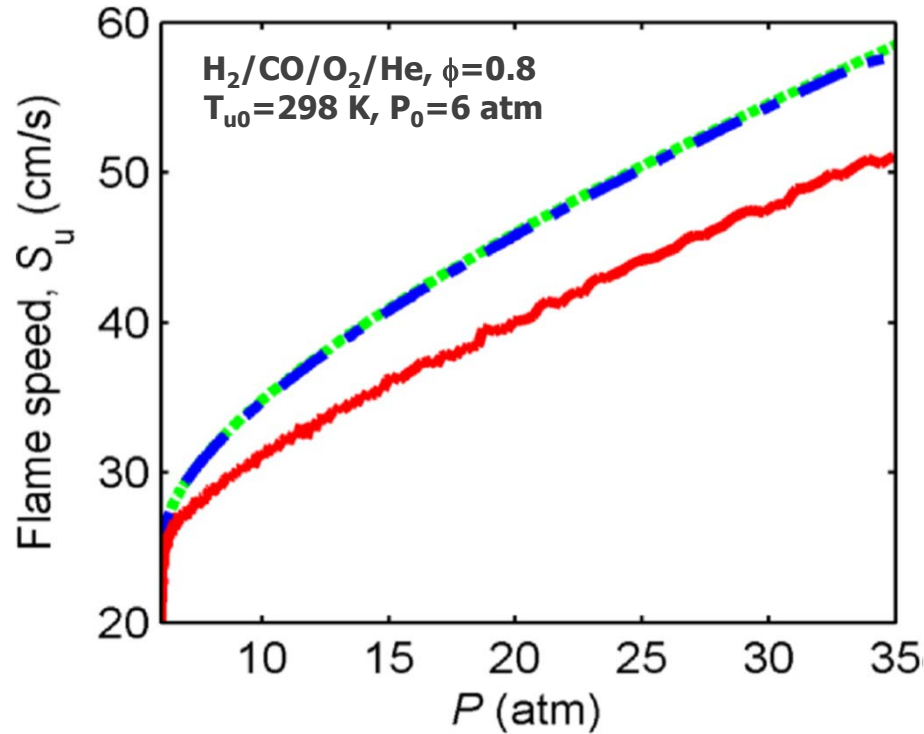
CH<sub>4</sub>/air,  $\phi=0.6$ , T<sub>u0</sub>=300 K, P<sub>0</sub>=1 bar



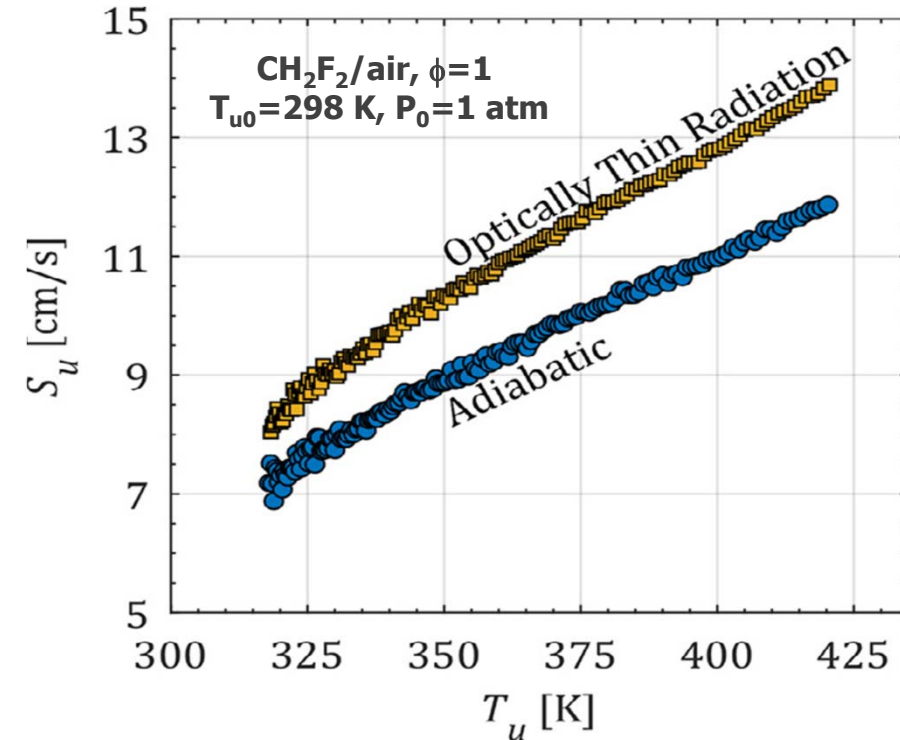
- Negligible even for weak mixture: **within 2%**
- Radiation **absorption** reduces the difference
- Slow burning fuels, e.g.: refrigerants ?

# Radiation

$$S_u = \frac{dR_f}{dt} - \frac{R_w^3 - R_f^3}{3P\gamma_u R_f^2} \frac{dP}{dt}$$



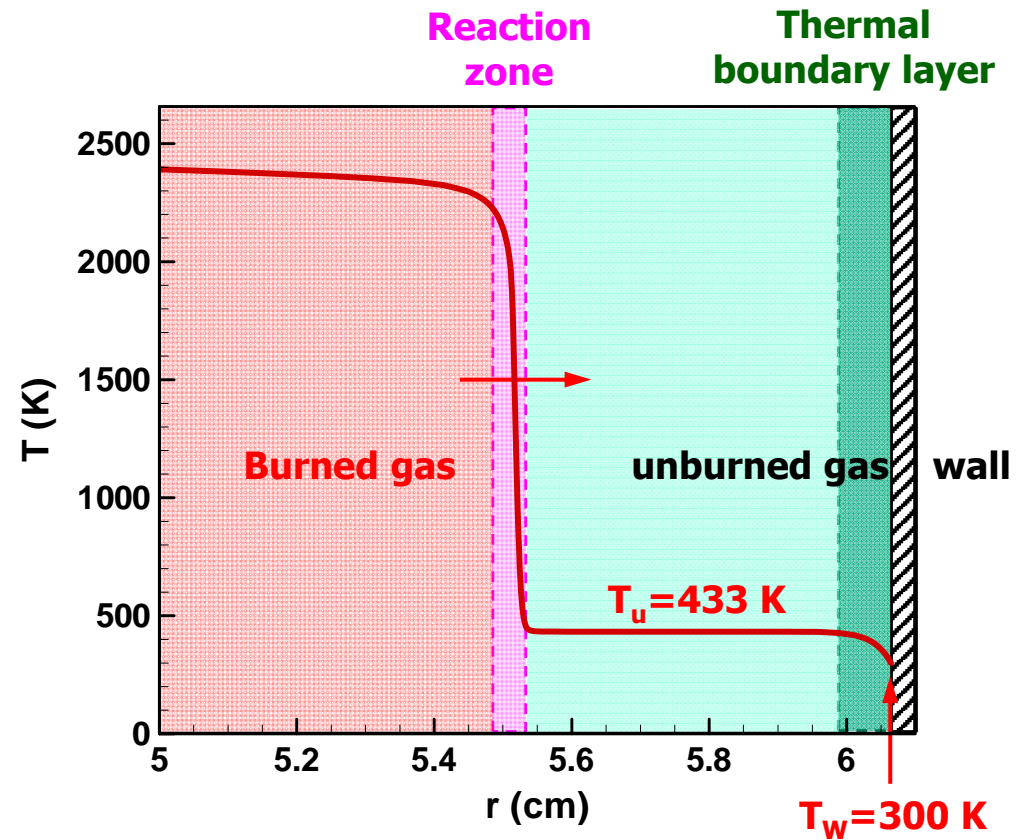
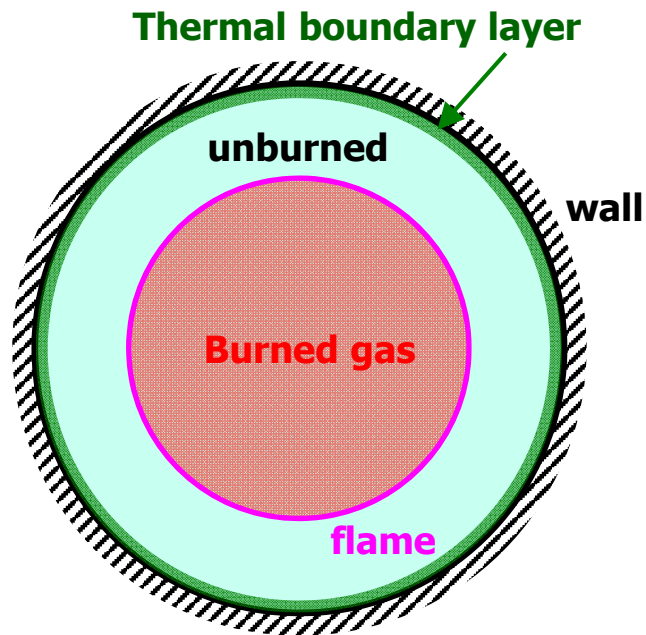
Xiouris et al. (2016CNF)



Burrell et al. (2019PCI)

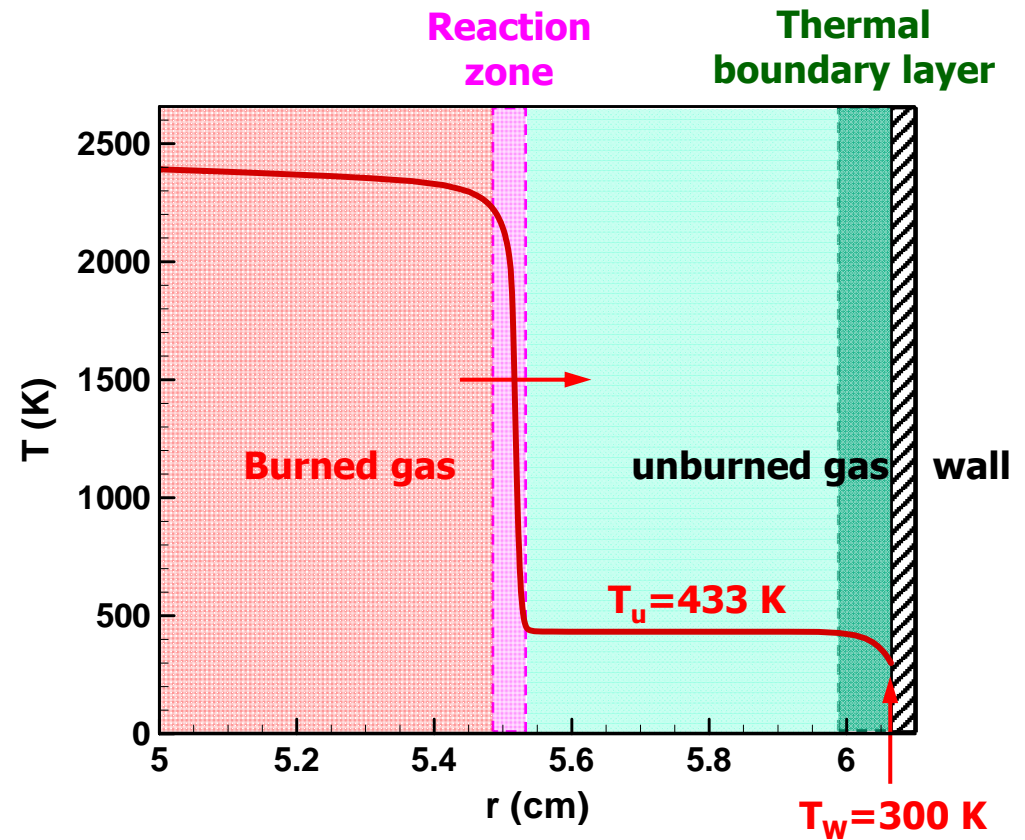
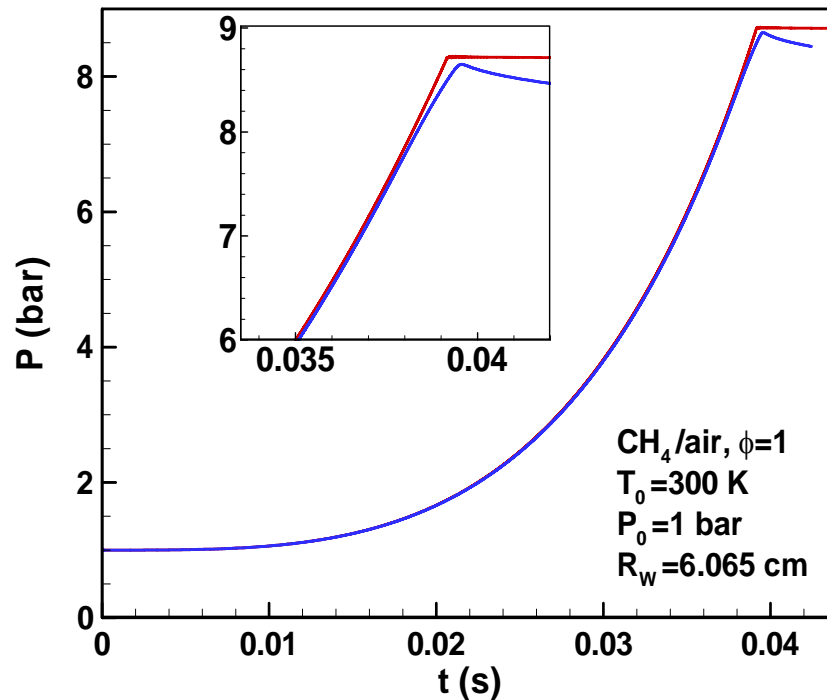
- “Neglecting radiation heat loss when interpreting experimental data could lead to uncertainty as large as **15%**”

# Wall heat loss



- A thin thermal boundary layer develops near the wall

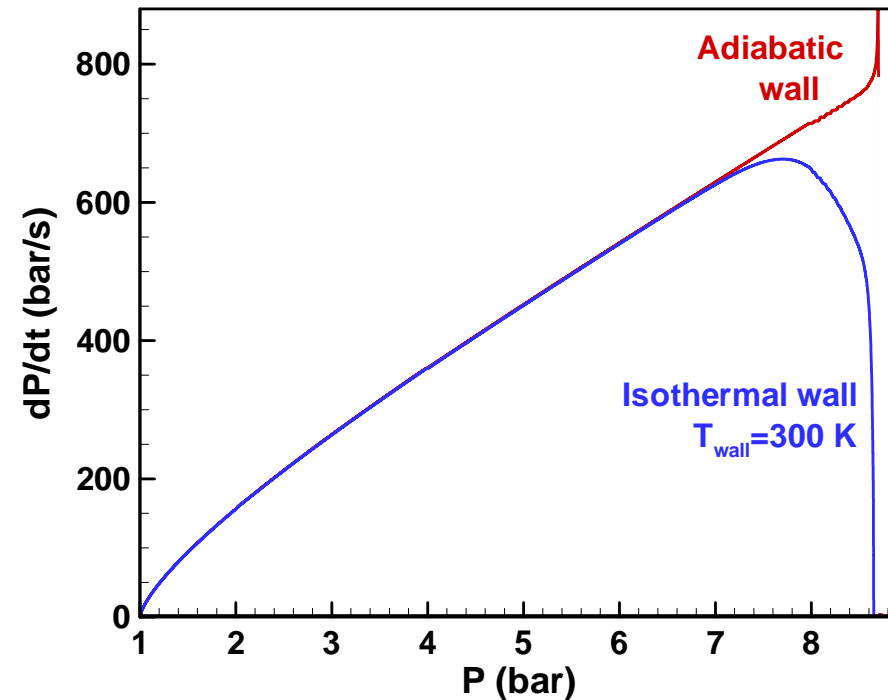
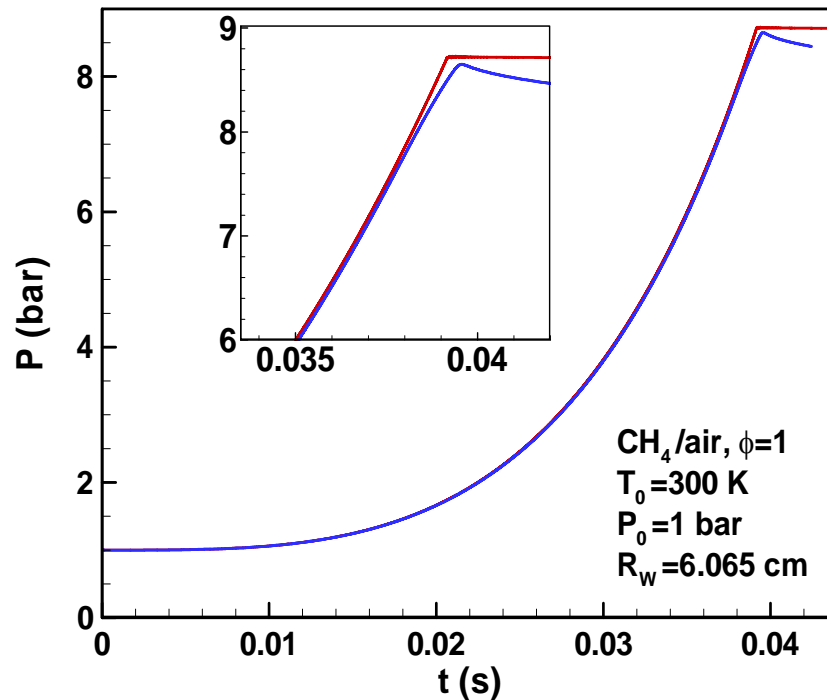
# Wall heat loss



- A thin thermal boundary layer develops near the wall
- Heat loss to the wall results in pressure drop



# Wall heat loss

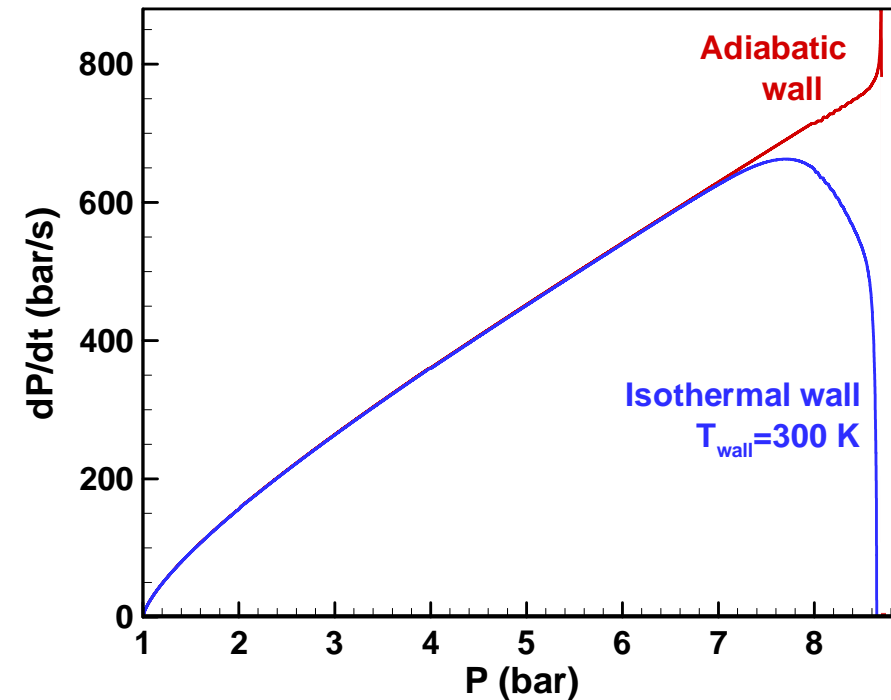
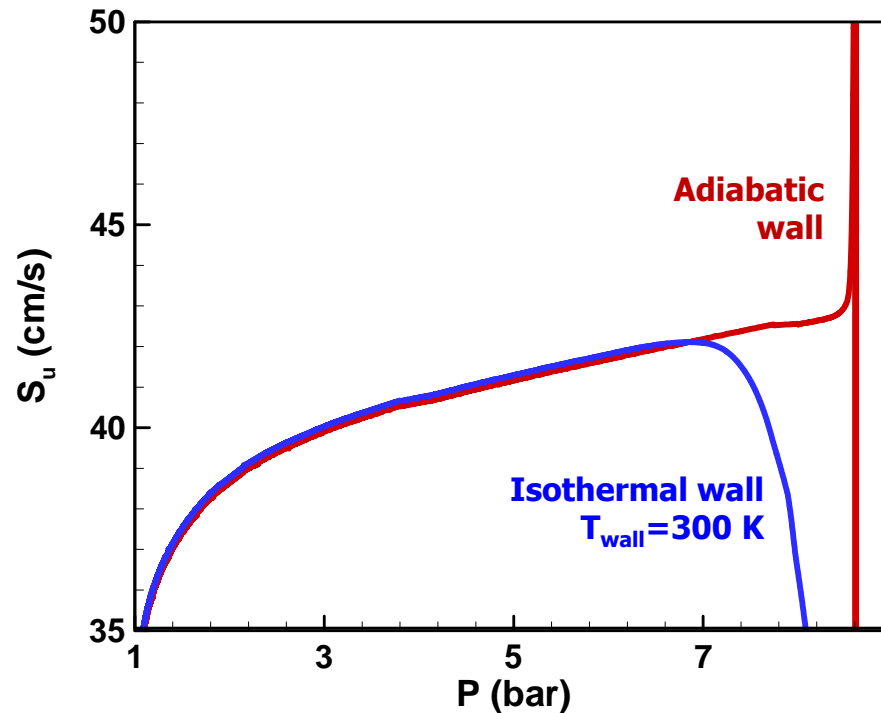


- A thin thermal boundary layer develops near the wall
- Heat loss to the wall results in pressure drop
- Useful data before  $(dP/dt)_{\text{max}}$



# Wall heat loss

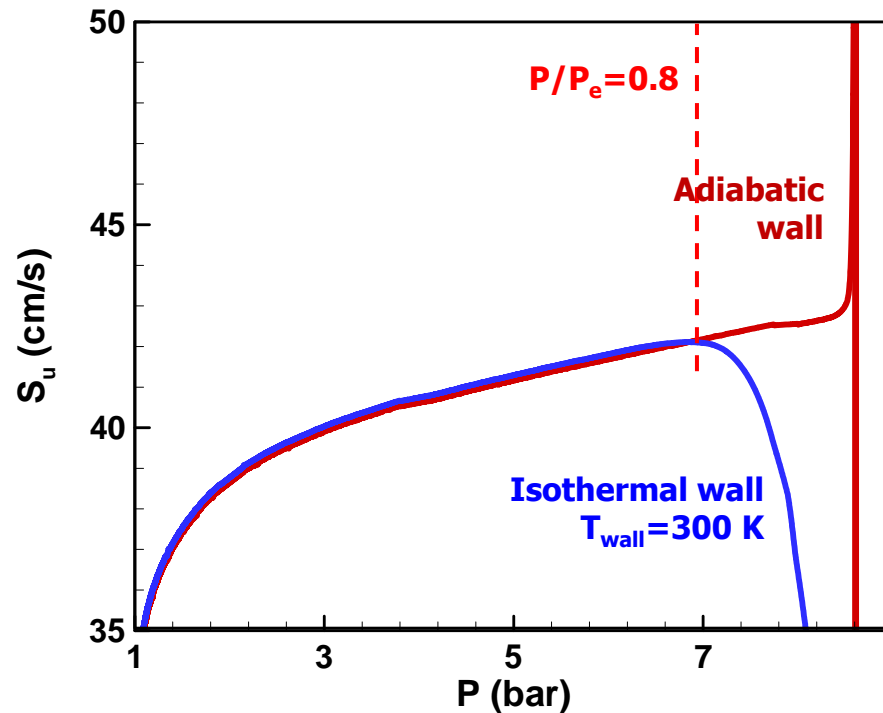
$\text{CH}_4/\text{air}$ ,  $\phi=1$ ,  $T_{u0}=300\text{ K}$ ,  $P_0=1\text{ bar}$



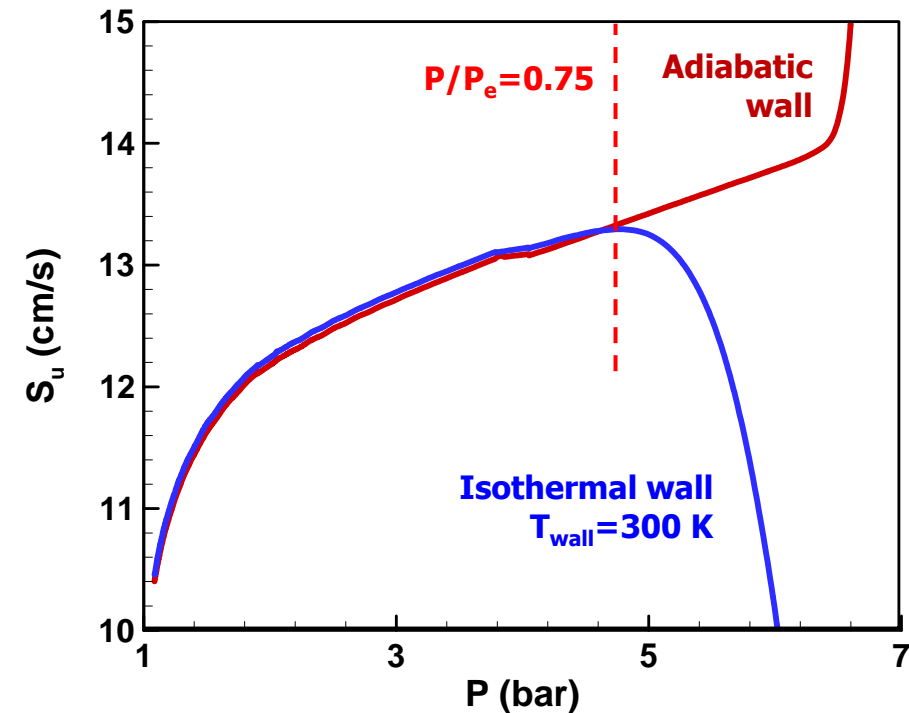
- A thin thermal boundary layer develops near the wall
- Heat loss to the wall results in pressure drop
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# Wall heat loss

CH<sub>4</sub>/air,  $\phi=1$ ,  $T_{u0}=300$  K,  $P_0=1$  bar

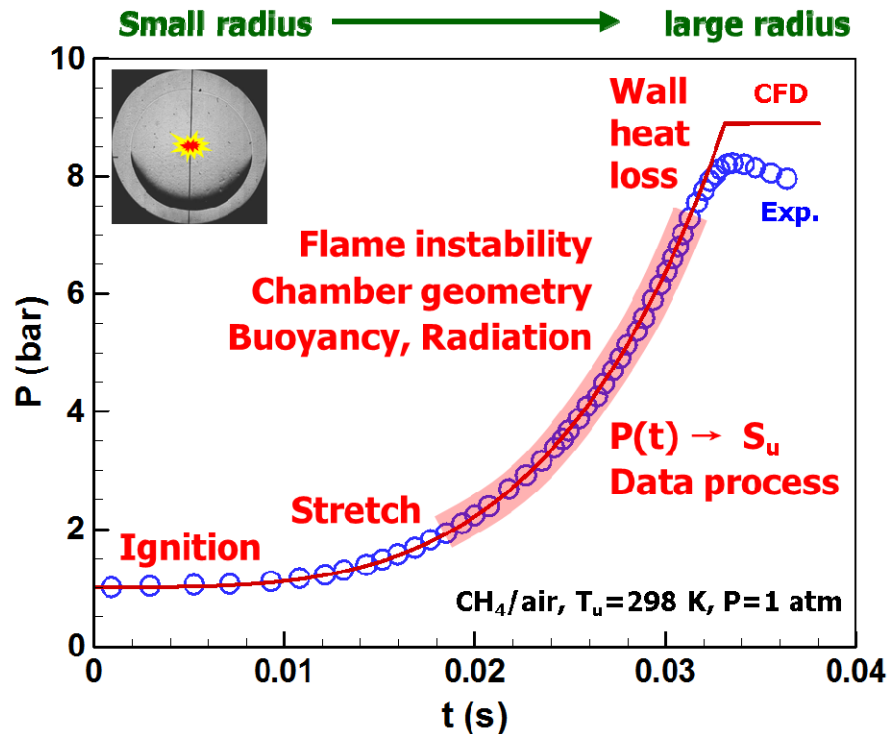


CH<sub>4</sub>/air,  $\phi=0.6$ ,  $T_{u0}=300$  K,  $P_0=1$  bar

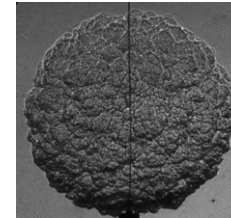


- A thin thermal boundary layer develops near the wall
- Heat loss to the wall results in pressure drop
- Useful data before  $(dP/dt)_{max}$

# Summary

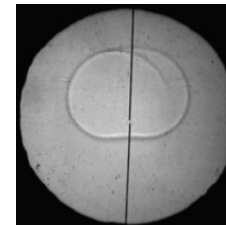


## Flame instability



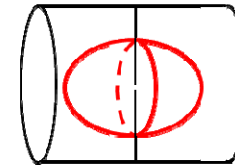
(Jomaas et al. 2013)

## Buoyancy

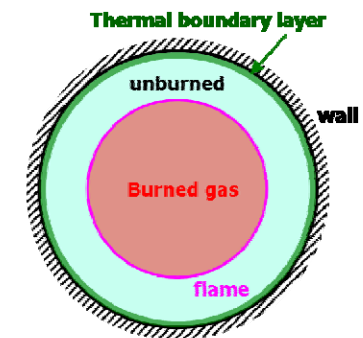


(Qiao et al. 2007)

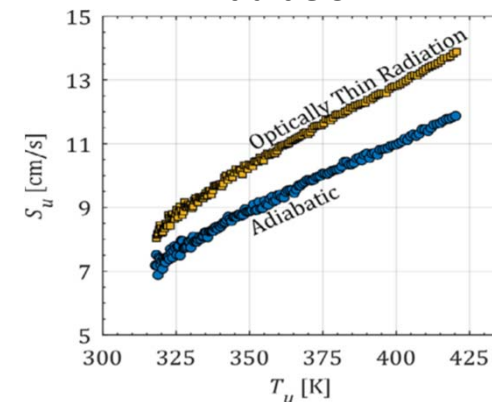
## Cylindrical chamber



## Wall heat loss



## Radiation



(Burrell et al. 2019)

- To avoid stretch effect:  $P/P_0 > 2$  or  $P > 5$  atm
- To avoid wall heat loss:  $P/P_e < 0.75$
- Negligible radiation effect for:  $S_u > 10$  cm/s ?
- Negligible buoyancy effect for:  $Ri = (T_b/T_u - 1)gL/S_u^2$  ?
- Data processing, burned mass fraction:  $x = m_b/m_0$

$$S_u = \frac{R_w}{3} \left[ 1 - (1-x) \left( \frac{P_0}{P} \right)^{1/\gamma_u} \right]^{-2/3} \left( \frac{P_0}{P} \right)^{1/\gamma_u} \frac{dx}{dt}$$

$$S_u = \frac{dR_f}{dt} - \frac{R_w^3 - R_f^3}{3P\gamma_u R_f^2} \frac{dP}{dt}$$



# Thank you !

## On laminar burning velocity measurement using the **constant-volume** propagating spherical flames

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